

To Treat or NOT?

38th Annual Corrosion Short
Course

EnhanceCo Inc
Lance Barton
Tom Pickthall
2026



This Should be Called.....
How Do I Design My Internal
Corrosion Program?

My Internal Corrosion Control Program



Oh (“_____”) I have evidence of Internal Corrosion

Not dealing with any Stress Corrosion-Stress Cracking Corrosion (SCC), Sulfide Stress Cracking (SSC), Hydrogen Induced Cracking (HIC),



What type of corrosion am I dealing with-Pitting/Uniform



Where are my risks – High Consequence Areas



Corrosion occurring – Top, Bottom, Throughout the line



How do I mitigate my internal risks

Know Your System

- Identify the corrosive constituents and environment of the product your moving – **Oil / Condensate, NGL**
 - Sulfur content - <0.5 wt% classified as sweet
 - TAN total acid number - >0.5 mg is considered high for crude oil
 - Paraffin/Asphaltene
 - BS&W
 - Continual or intermittent flow
 - Flow velocities when pumping
 - General topography – where are the low spots
 - History of leaks

Know Your System

- Identify the corrosive constituents and environment of the product your moving – **Gas**
 - CO₂, H₂S, O₂ content
 - Flow velocities = Flow pattern (where's the water)
 - General topography – where are the low spots – water and deposits
 - History of leaks / cut-outs

You Have
Identified
the Issue –
What are
the Possible
Solutions?

- Physical
 - Pull liners / Coated pipe
- Operational (Make changes to the system)
 - Pigging
 - Change Velocities
 - Higher velocities to help sweep water from low areas
 - High velocities can increase solids impingement
 - Pressures
 - Increase/Decrease pressures to change velocities and flow patterns
 - Intermittent Flow to Continuous Flow – Oil/Liquids

Possible Solutions

- Change the Water Content and Quality of Crude or Gas
 - Tighter control on BS&W
 - Dehydration System
 - Molecular sieve
 - CO₂, H₂S scavenger Towers
 - O₂ Tighter control of what we are buying – hydrate inhibitor/less methanol
 - Amine Unit

Possible Solutions

Possible Solutions

- Make the Lines piggable
 - Install launcher / receiver
 - Argus Pigging Valve
 - Create and maintain a pigging schedule
 - Use the appropriate type of pig for the job



Modernize Your Pigging Stations.

Possible Solutions

What type(s) of internal corrosion have I identified/suspect and therefore plan to mitigate or reduce to acceptable levels

Pigging if possible is an important mitigation method

- Proper pig selection to remove water/liquids and deposits
- Pigging in conjunction with chemical treatments
 - Effectively distributes chemical thorough the line
 - Spray pigs to apply chemicals to the top of the line

Possible Solutions

- Move the coupons and monitoring tools to areas in the line that won't show high corrosion rates! (No – please don't do that...)

Or

- Start and monitor a chemical treating program
 - What do I need to use
 - How often
 - At what dosage
 - How am I going to apply it
 - How am I going to prove my program is working
 - Do I have background data?



Solutions – Chemical Application

Common Chemical Application Methods

- Continuously inject a calculated amount of chemical
 - Scavengers – CO_2 , H_2S
 - Scrubbers / Amine Units a more economical option most of the time
 - Continuously injecting scavengers may have other side effects
 - Paraffin solvents / Paraffin inhibitors
 - DRA's
 - Emulsion Breakers
 - Antifoulants and Cleaners
 - Corrosion Inhibitors and Biocides

Chemical Application Methods

- Continuously inject a calculated amount of chemical
 - Corrosion Inhibitors
 - Must have enough velocity to carry inhibitor through the line
 - Will be chosen for the method of dispersion (water soluble, oil soluble, dispersable, etc)
 - Need a monitoring method to assure the inhibitor gets to the end of the line at a sufficient quantity to be protective-residuals
 - Biocides
 - Not typically recommended for continuous injection in pipelines unless lines are pigged
 - Intermittent injection can be used to treat tanks and sump
 - Contact time is a key variable
- Pigging operations may affect continuous injection inhibition films

Common Chemical Application Methods

- Batch chemical treatments with pigs
 - Corrosion inhibitors, Paraffin cleaners, Biocides, Line cleaning chemicals
- Chemical pill batched between two pigs
 - Chemical pill volume calculated to cover surface area of the pipe
 - Used with oil solubles to “coat” the entire circumference of the pipeline
 - Used if there is a potential for top of the line corrosion
- Chemical pill batched in front of pig
 - Chemical pill volume calculated to cover surface area of the pipe
 - Often used with surfactants to “lift” solids in front of the pig
- Chemical pill batched behind a pig
 - Used with biocides to allow more contact time
 - Used with water soluble products

Common Chemical Application Methods

- Slug Treatments
 - Treatment volume calculated and pumped into the line
 - Treatment typically diluted with solvent or water
 - Chemical volume is calculated to be enough to cover the length of the line
 - Slug treatments are used primarily on non-piggable lines
 - It is hard to get uniform coverage

Corrosion Inhibitor Selection

Corrosion Inhibitor selection depends on what is being transported, what type of corrosion I am trying to mitigate, where are the areas the corrosion is of concern

- Oil and other liquid products
 - Water, Paraffin/Asphaltene content, density
 - Flow velocities – laminar, transitional, turbulent
 - Continuous flow vs intermittent flow
 - Compatibility with system fluids and downstream processes
 - Application – Batch, Slug or Continuous injection

Corrosion Inhibitor Selection

Corrosion Inhibitor Selection

- Natural Gas
 - Water content (lbs/mmcf)
 - Flow velocities – flow pattern
 - Temperatures – gas temp vs pipe temp – TLC
 - Compatibility with system fluids and downstream processes
 - Application – Batch, Slug or Continuous injection

Biocide Selection

Biocide selection depends

- Oil and other Liquid Products
 - BS&W content
 - Time Kill Studies – Contact time with biocide/concentration of biocide
 - Source of bacterial intrusion – sumps, tanks contamination
 - Compatibility with system fluids - DRA
 - Application – Batch or Slug
 - Usually best to treat the source if possible

Biocide Selection

Biocide selection depends

- Natural Gas
 - Water content –lbs/mmcf
 - Time Kill Studies – Contact time with biocide/concentration of biocide
 - Source of bacterial intrusion – Drips, Laterals feeding certain line(s)
 - Compatibility with system fluids
 - Application – Batch or Slug
 - Usually best to treat the source

Corrosion Inhibitor Types

Corrosion Inhibitors

Most common are nitrogen based polar amines-attracted to the metal surface

- Water soluble – Soluble in water phase
 - Form a barrier between aqueous phase and pipe surface
- Oil soluble – Soluble in oil phase
 - Used widely where water is the only liquid phase, or there is very little free water
 - Generally have a greater film persistency (sometimes called Gunkers)
- Oil soluble / Water dispersible
 - Soluble in oil phase, yet disperses into the water phase
 - Widely used in crude lines

Corrosion Inhibitor Types

One-off Corrosion Inhibitor Treatments

Some binary corrosion inhibitors have a greater film life

- Two-part inhibitors once mixed have an application window – curing time
- Must be applied using pigs
- Storage fields where lines can only be treated certain times throughout the year
- Bi-directional flow lines – small window to treat line(s)
- Aggressive pigging cannot be used with this mitigation method

Corrosion Inhibitor Types

One-off Corrosion Inhibitor Treatments-Gas

Un-piggable line treatments on low flow wet gas lines
– gathering lines primarily

- Designed to treat to the entire length of the line
- Slug treatment
- Treatment volume calculated based on 15-20% line fill
- Slug treatment consists of corrosion inhibitor, biocide and or a foamer
 - The foamer or biocide helps to carry the treatment to the end of the line
- Benefits
 - Distributes treatment to the end of the line
 - Helps unload the stagnant water from the line

Components To Monitor

pH and Alkalinity

- Corrosivity of the water

Deposits

- Periodic analysis of deposits tell us what the corrosion by-products are

Bacteria

- Planktonic and Sessile

Coupons

- Corrosion rates – general mpy and pitting mpy

Chlorides

- Periodic check of the salinity of the water

Iron and Manganese

- Test for changes upstream and downstream, as well as the ratio of Fe/Mn (roughly 50:1)

Scaling Tendency

- Test for potential scale formation (both acid soluble and acid insoluble scales)

Monitor System and Program Changes

Monitor changes when you make changes to the mitigation program

- Started or changed a pigging program
 - Are the solids analysis generally the same
 - Is there a decrease in the amount of solids
- Increased/decreased amount of gas / oil moving through the line
- Added laterals feeding line
 - Monitor the quality of new or added
- Started or changed a chemical program
 - Coupon mpy's/pitting mpy's improved to acceptable levels
 - Bacteria counts improve
 - Chemical residuals
 - Solids increase or decrease



Lance Barton
EnhanceCo Inc.

LanceBarton@Enhanceco.net

417.204.1614 Cell

281.499.4426 Office



THANK YOU FOR
YOUR LISTENING

DO YOU HAVE
ANY QUESTIONS?

- Tom Pickthall
- EnhanceCo Inc.
- Tomp@Enhanceco.net
- 713.906.4841 Cell
- 281.499.4426 Office